

A novel method for controlling heat exchangers

Presentation to the 8th Meeting of the Process Intensification Network

14th November 2002

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M Conventional temperature control

Example: Batch vessel with internal cooling coil...

... undergoes a step change in heat load





Conventional temperature control

Example: Batch vessel with internal cooling coil...



... the temperature rise of the process is corrected by varying the cooling coil loading



M Heat balance measurement

... the cooling fluid temperature is varied to **Example: Measuring a heat** balance across the to control the process fluid temperature coil... **Cooling Fluid Temperature** 10 Fluid out Fluid in Temperature (°C) 9 8 7 6 5 2 0 4 6 8 10 Time (seconds) TC Process heat load 10 kW

Coolant flow 10 kg/s

M Heat balance measurement





Conventional "Fixed Area" control





Example: The same 10kW step change in heat load



... process temperature control is quicker and more stable **Process temperature** Fast response due to very cold 14 temperature of cooling fluid Temperature ⁰C 13 No overshoot due to capacity 12 limits imposed by heat 11 transfer area 10 9 8 2 6 8 10 0 Δ Time



Example: Measuring the heat balance across the <u>"on/off"</u> coil



... the cooling fluid temperatures look quite different





Example: Measuring the heat balance across the <u>"on/off"</u> coil

... the subsequent heat balance is very accurate







How can a heat exchanger be designed which matches heat transfer area to heat load at constant LMTD?

N Patented "variable area" jacketed reactor design







Ashe Morris is exploiting this patented concept to develop better heat exchangers across a number of applications



M Benefits of "variable area" control

Existing batch reactors

Process intensification

- Improved yield quality and safety from on-line reaction monitoring and better temperature control.
- Smaller reaction volumes
- Stable temperature control at higher thermal gradients
- Faster temperature control
- Accurate enthalpy data for online monitoring
- Transition from batch to continuous



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