

Laboratory Protocol of PI

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Aims and Benefits of PI?

Provide equipment that enables the process chemistry to proceed at its optimum kinetic rate, with minimal by-products, resulting in plant which is: -

Safer, Smaller, Cleaner, Faster

Results in:-

- ◆ Higher product yield and less waste
- ◆ Smaller inherently safer plant
- ◆ Lower capital and running costs



Constraints of PI

Numerous constraints, restricting the use of Process intensification in industry:

- ◆ **Reaction kinetics**
- ◆ **Processing solids**
- ◆ **Process size ('Biggest is best' philosophy)**
- ◆ **Lack of awareness**
- ◆ **Limitations of product variability**
- ◆ **Uptake novel technologies**
- ◆ **Timescales**
- ◆ **Resistance to change**



PI Methodology

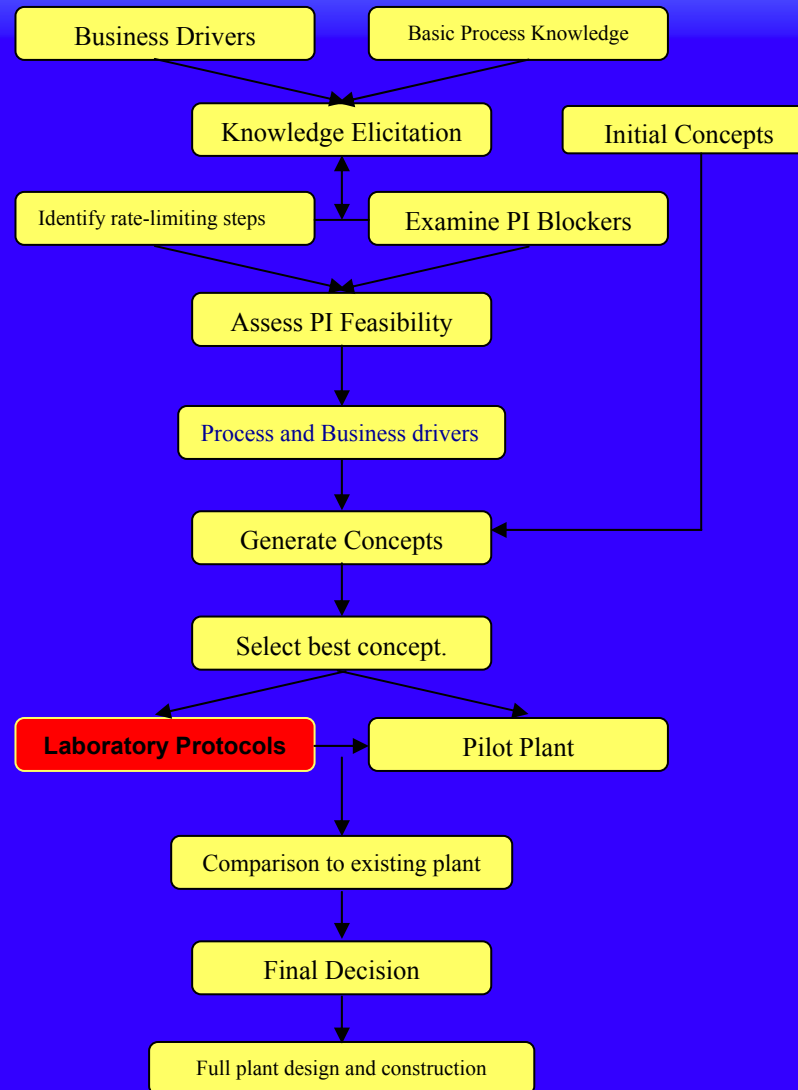
In an attempt to overcome these constraints, BHR group developed a PI Methodology

This allows the suitability of process for intensification by assessing:

- ◆ **Business Drivers**
- ◆ **Basic process knowledge**
- ◆ **Currently available or novel PI technology**

Within the methodology was a 'Laboratory Protocol' section

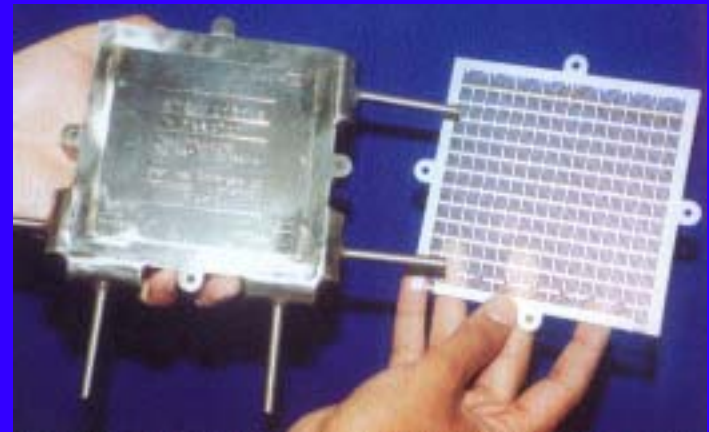
PI Methodology



Laboratory Protocol

PI is difficult to model within the laboratory as there exists an inability of small scale experiments to recreate the conditions experienced in a PI plant.

Design a small high intensity stirred tank reactor...



...to try and simulate and model intensified reactor systems

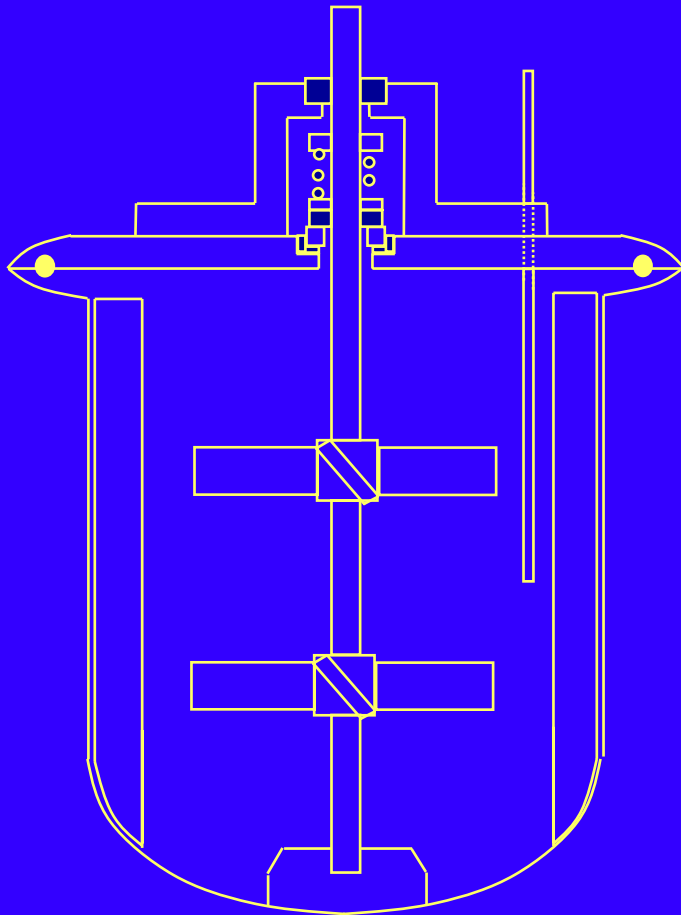


Design of the Vessel

Design considerations for construction of the protocol vessel: -


- ◆ **High intensity mixing**
- ◆ **Homogenous mixing**
- ◆ **Heat transfer capabilities.**
- ◆ **Simple to use**
- ◆ **Safe to use**
- ◆ **Well understood**

Protocol Vessel



Protocol vessel consists of:-

- ◆ 733ml glass vessel
- ◆ baffles
- ◆ Dual 45° PBT's
- ◆ 0- 4000 rpm Motor
- ◆ Mechanical shaft seal



Why use Laboratory Protocol?

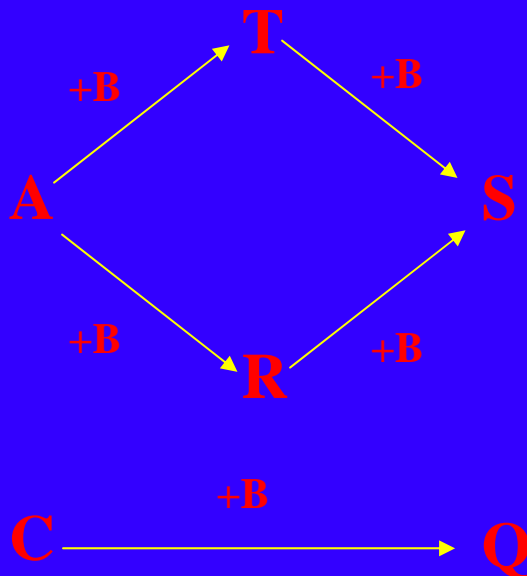
Industry needs to be shown that PI is a viable option for its processes but why use laboratory protocols, rather than demonstration rigs of intensified equipment?

- ◆ **Less process fluid requirement.**
- ◆ **Quick and Simple**
- ◆ **Uses 'known' equipment.**
- ◆ **No risk of fouling or blocking.**

Bourne Reaction Scheme

The mixing characteristics of the vessel were tested using the 'mixing sensitive' Bourne reaction scheme.

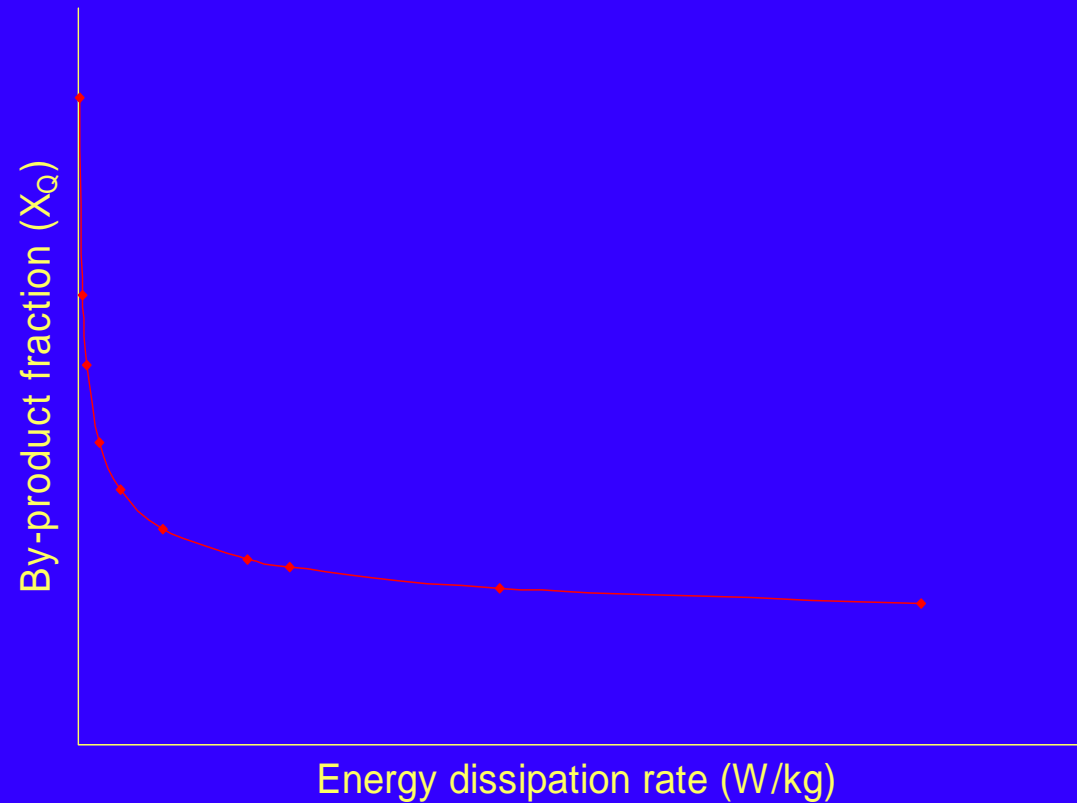
Involves mixing of a solution of 1-Naphthol (A) and 2-Naphthol (C) and diazotised sulphanic acid (B)



- ◆ If mixing is perfect, the faster reactions are favoured, so mostly R will be formed
- ◆ If mixing is not perfect, the faster reactions are mixing-limited and more by-products, S and Q, are formed.

Bourne reaction scheme

The by product fraction, X_Q , is used as a measure of the degree of mixing.





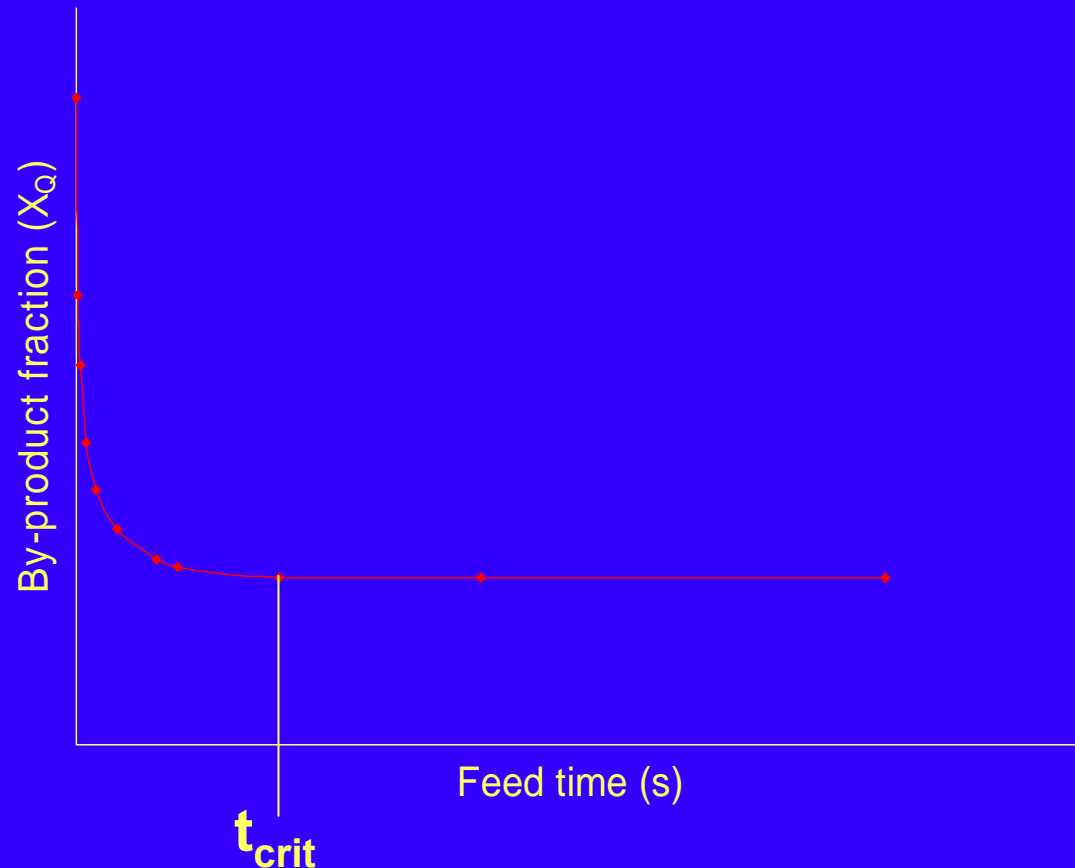
Characterisation

Protocol vessel was characterised: -

- ◆ **Power number determination for dual impeller.**
- ◆ **Heat transfer capabilities.**
- ◆ **Effect of impeller arrangement.**
- ◆ **Effect of impeller pumping direction.**
- ◆ **95% mix time determination.**
- ◆ **Local point energy dissipation rates (ϵ).**
- ◆ **Critical feed time analysis.**

Critical Feed time

Experimental determination of the critical Feed time:



Intensified Reactors

Why choose static mixers?



- ◆ Very common form of intensified plant/process.
- ◆ Used as both mixers and reactors.
- ◆ Well understood.
- ◆ Lot of data from HILINE experiments to model them with.

Static Mixers

What are they?

- ◆ Series of stationary guiding elements inside a pipe.



How do they work?

- ◆ Pumps delivering components supply the energy for mixing
- ◆ Stationary guiding elements in the pipe, split, divide and remix the fluid, at the expense of a pressure drop.

Static mixer simulation

Simulated four types of static mixer:



Kenics



SMXL



SMV



HEV



Process of simulation

- ◆ **Bourne reaction scheme in a static mixer system.**
- ◆ **Calculation/determination of mixing characteristics of Static mixer system**
- ◆ **Determination of process variables required to match those calculated for static mixer system.**
- ◆ **Bourne reaction scheme in Protocol vessel at determined process variables.**
- ◆ **Comparison of by product fractions obtained**

Simulating static mixers

Simulation involved matching one or several of the following characteristics:

- ◆ **Energy dissipation rates (ϵ)**
- ◆ **Reynolds number (Re)**
- ◆ **Mixing timescales**
 - ◆ **Macromixing (τ_{macro})**
 - ◆ **Mesomixing (τ_{meso})**
 - ◆ **Micromixing (τ_{micro})**

Simulating static mixers

Matching characteristics within the two systems:

	Static Mixer	STR
Energy dissipation rate	$\varepsilon_{AV} = f(\bar{u}^3)$	$\varepsilon_{AV} = f(N_i^3)$
Reynolds number	$Re_H = f(u)$	$Re_i = f(N_i)$

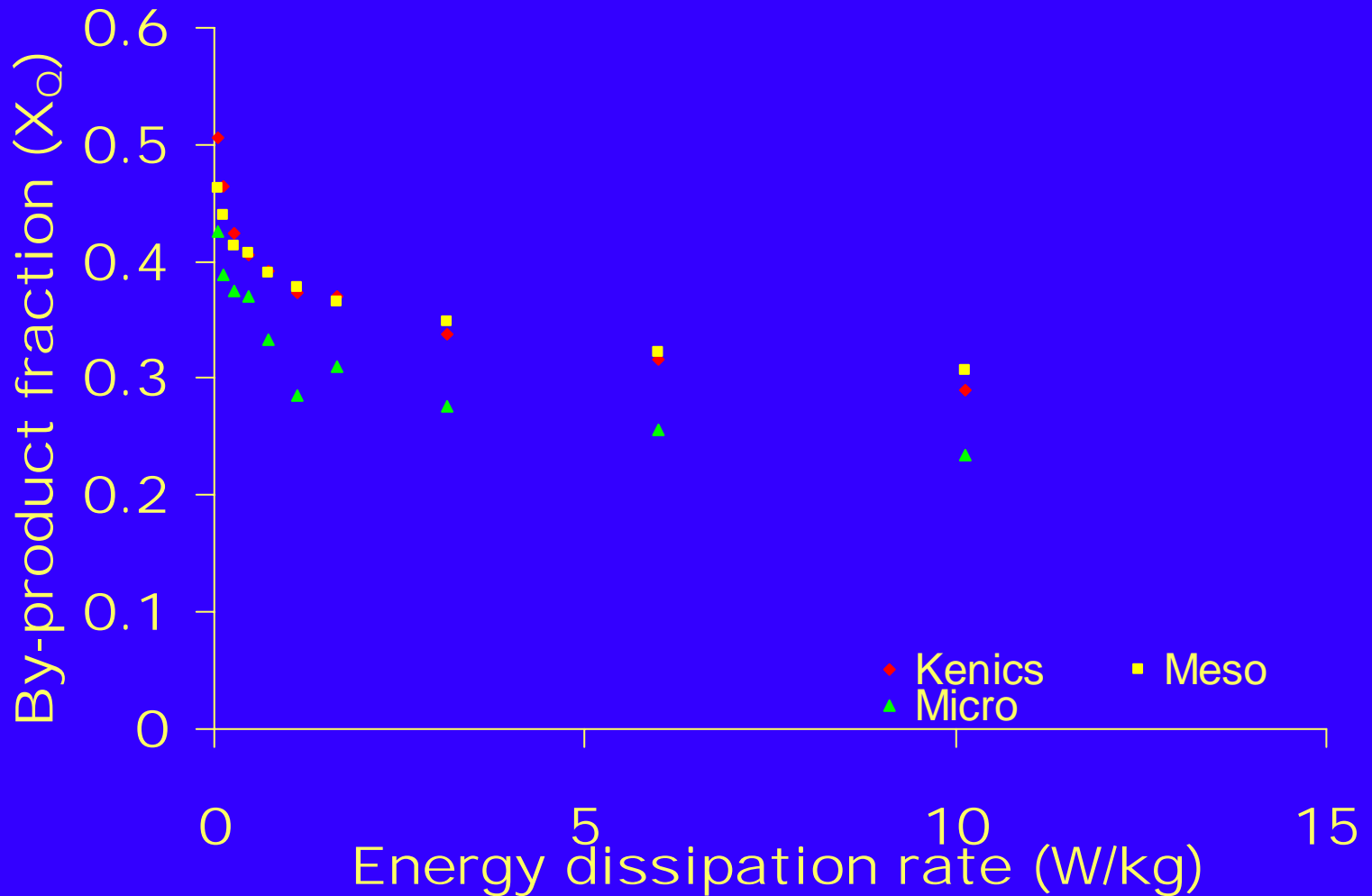
Simulating static mixers

Matching characteristics within the two systems:

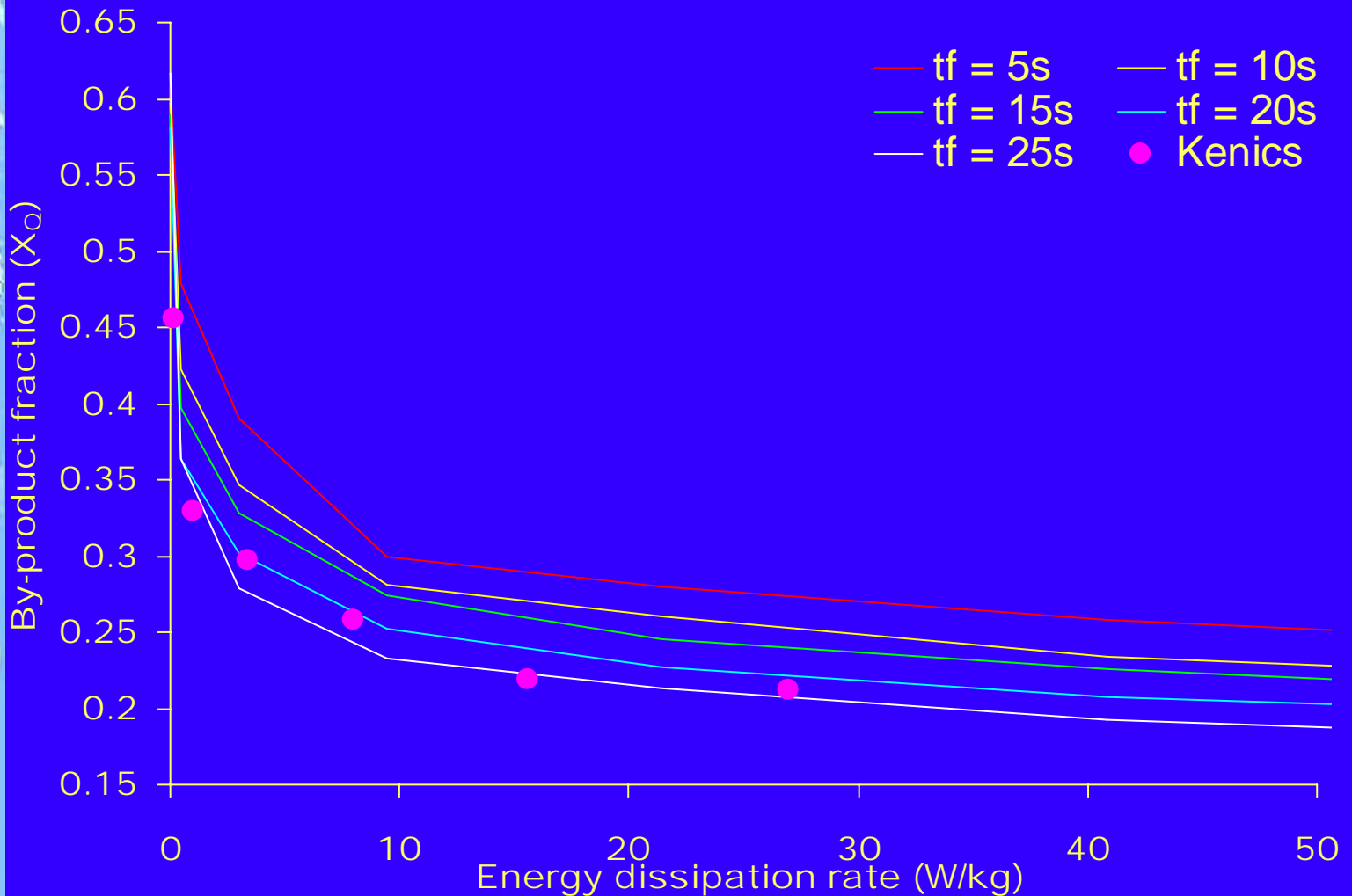
	Static Mixer	STR
Mesomixing timescale	$\tau_{\text{meso}} = f(Q_B \bar{u} \varepsilon)$	$\tau_{\text{meso}} = f(t_f, N_i)$
Micromixing timescale	$\tau_{\text{micro}} = f(v, \varepsilon)$	$\tau_{\text{micro}} = f(v, N_i)$

Initial Modelling

Initial modelling attempts:

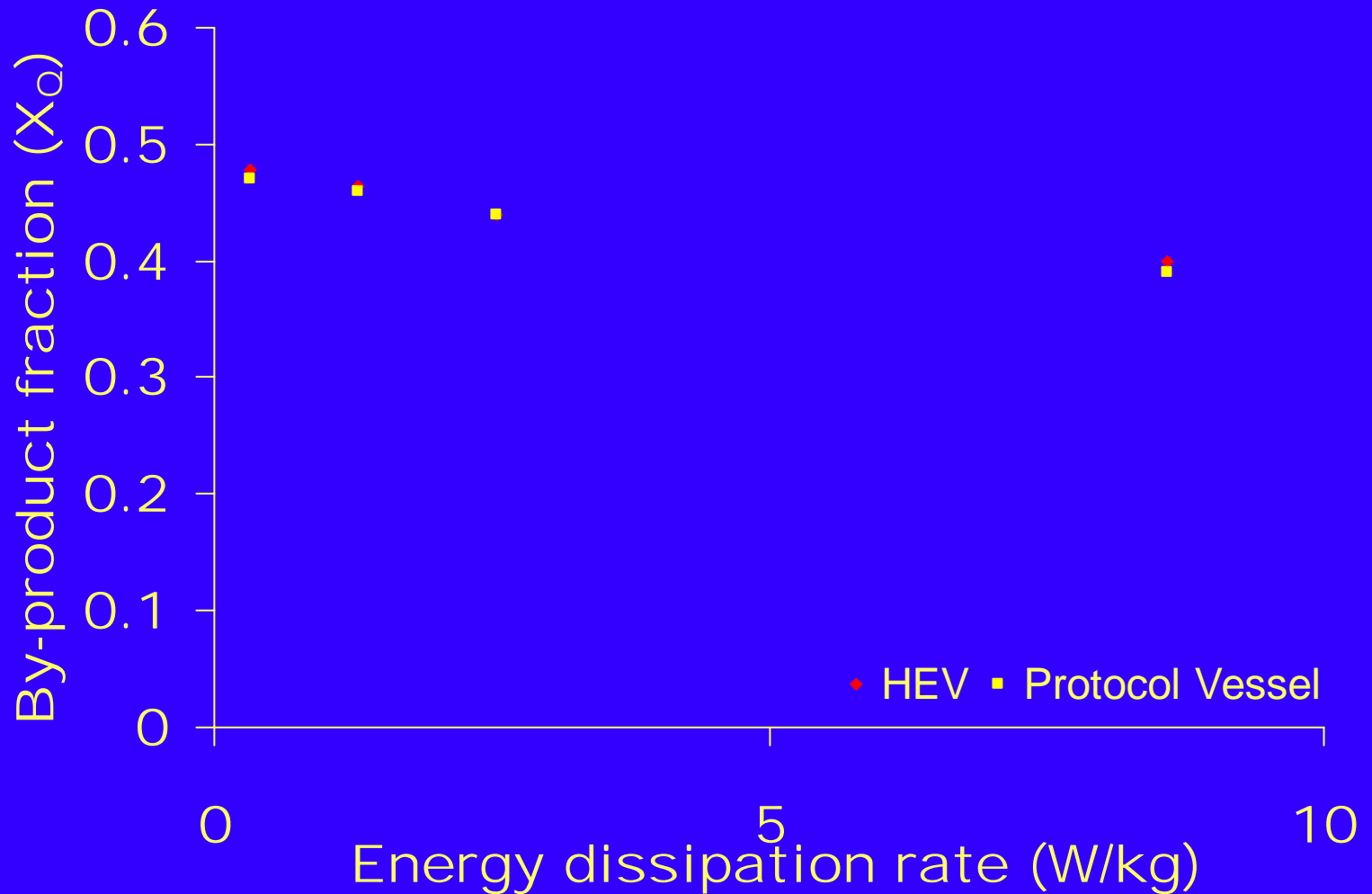


'Matrix' approach



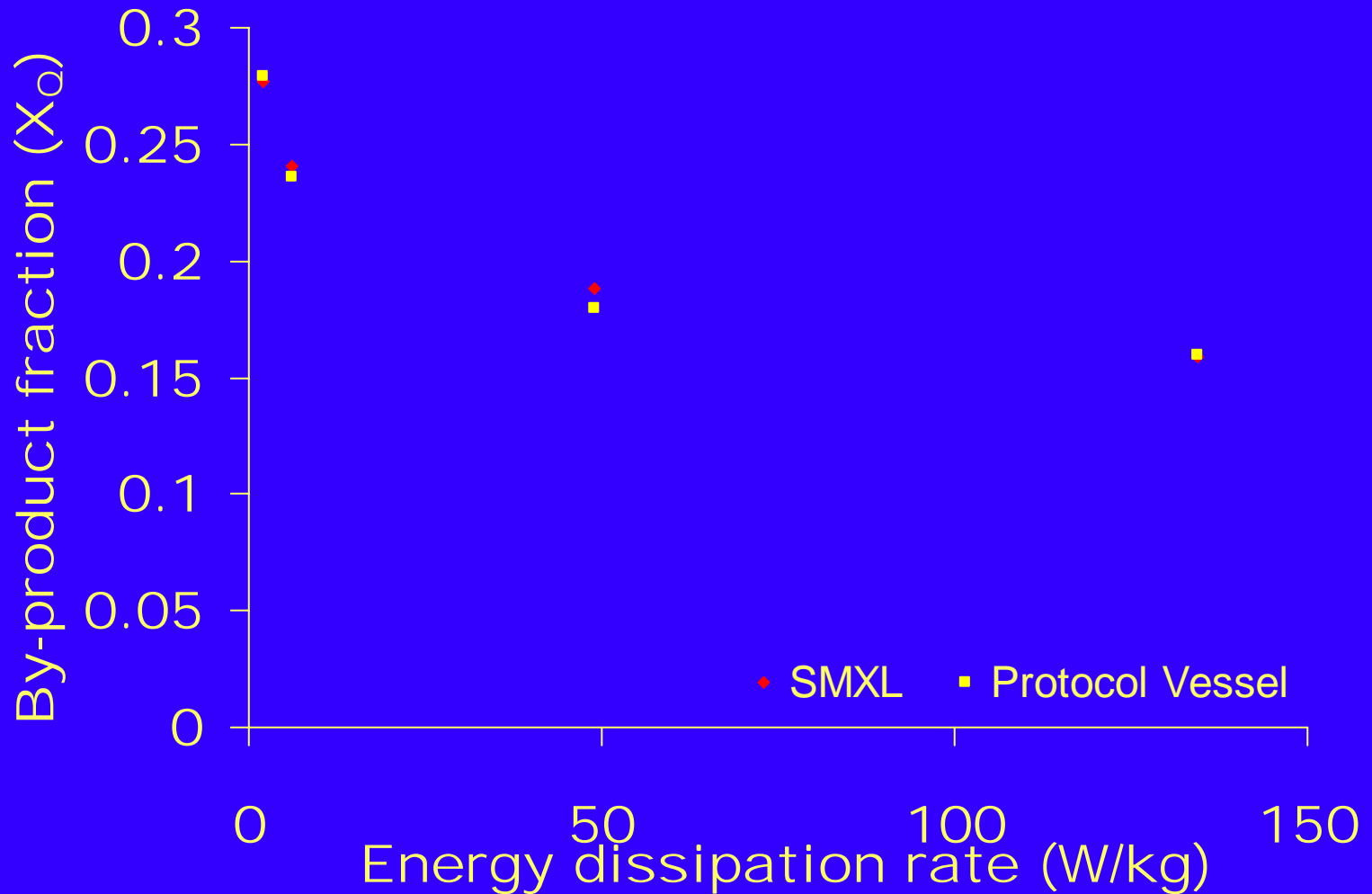
Static mixer simulation

HEV Static mixer - 7 Tab arrays



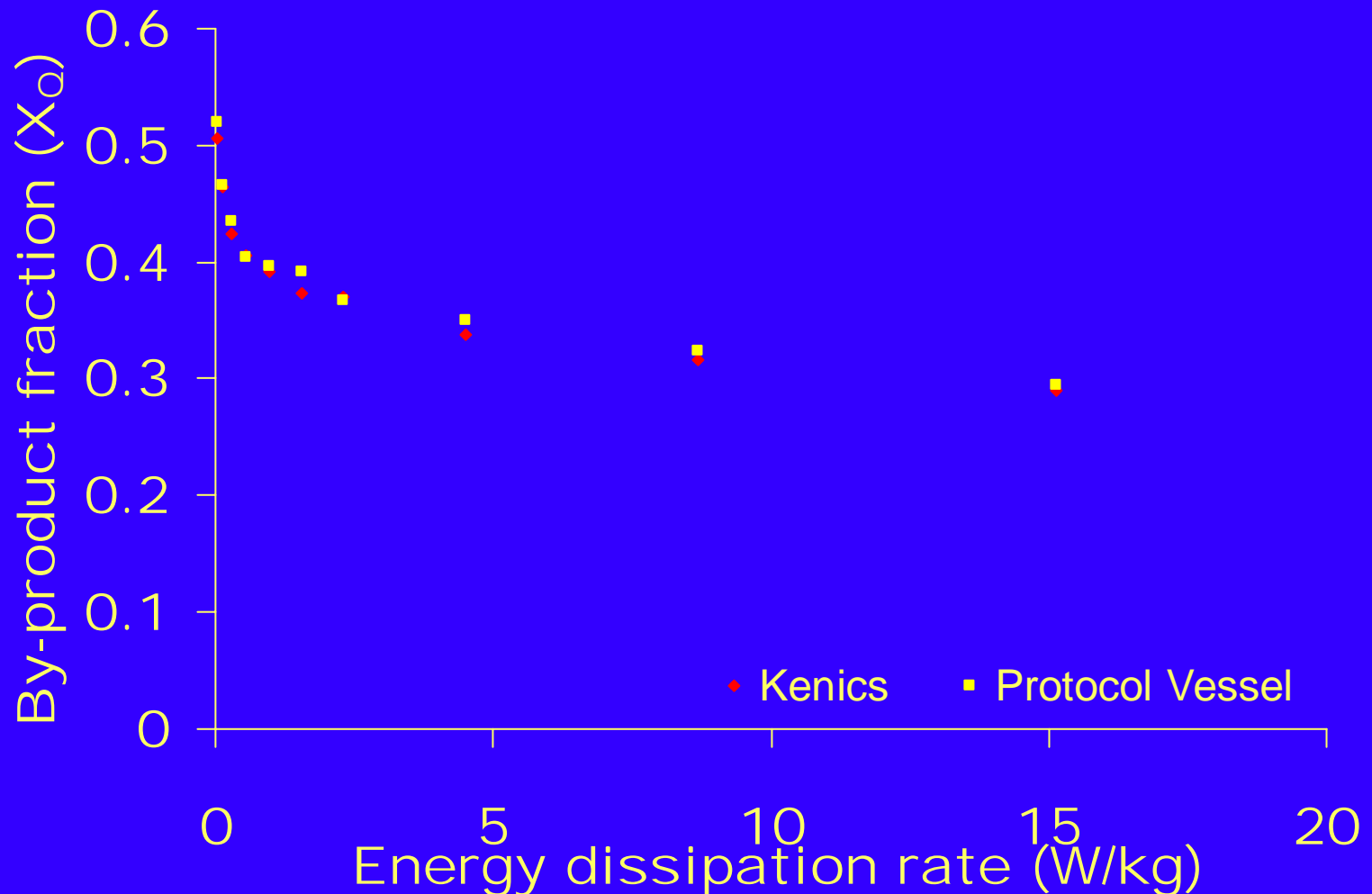
Static mixer simulation

SMXL Static mixer - 3 elements



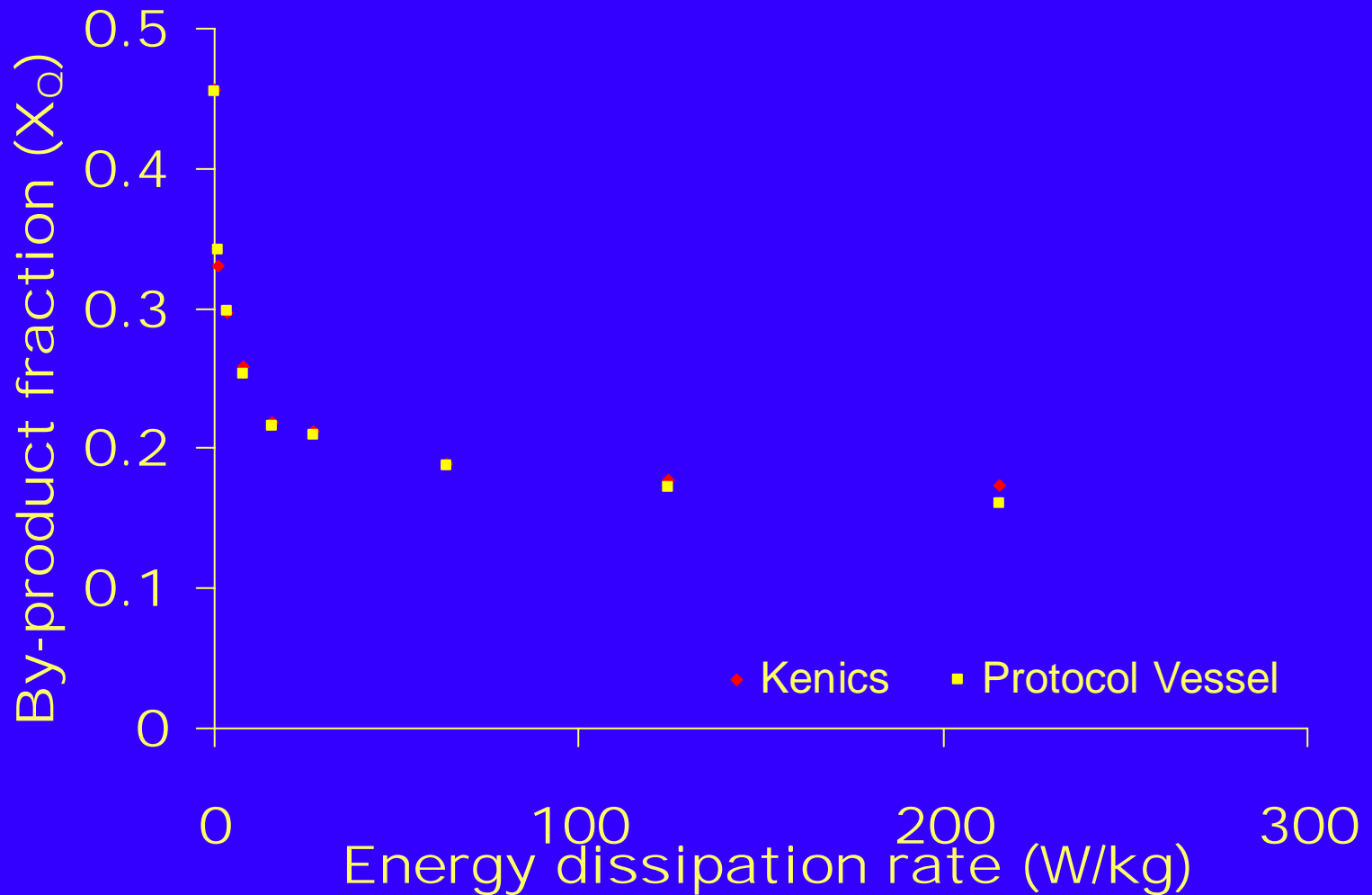
Static mixer simulation

Kenics Static mixer - 11 elements



Static mixer simulation

Kenics Static mixer - 9 elements





Conclusions

A reasonable match of the by-product fractions between the two systems can be obtained by:-

- ◆ **Setting Energy dissipation rate in the protocol vessel equal to that in the Static mixer system**
- ◆ **Estimation of a feed time from experimental matrix**



Future Work

- ◆ **Determine correlations between the two systems.**
- ◆ **Construction of methodology**
 - ◆ Allow selection of static mixer system from a series of bench scale STR tests
- ◆ **Use of other reaction schemes**
 - ◆ Single phase
 - ◆ Two phase
- ◆ **Simulation of other continuous systems**
 - ◆ HEX Reactors
 - ◆ spinning disks