



Intensification of the Steam Cracking Process

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Does Steam Cracking Need Steam



Presentation outline

- Introduction
- Catalytic plate reactors
- Coke formation
- Objectives
- Benefits
- Methodology
- Experimental Work
- Results
- Conclusions



Introduction

Olefins demand in year 2005 :

Ethylene (107 million tons)

propylene (67.1 million tons)

Olefins demand growth during years(2005 –2010):

Ethylene about 4.3% per year

propylene about 5.4% per year

Olefins production capacity growth:

Ethylene about 5.4% per year

Propylene about 5.1% per year

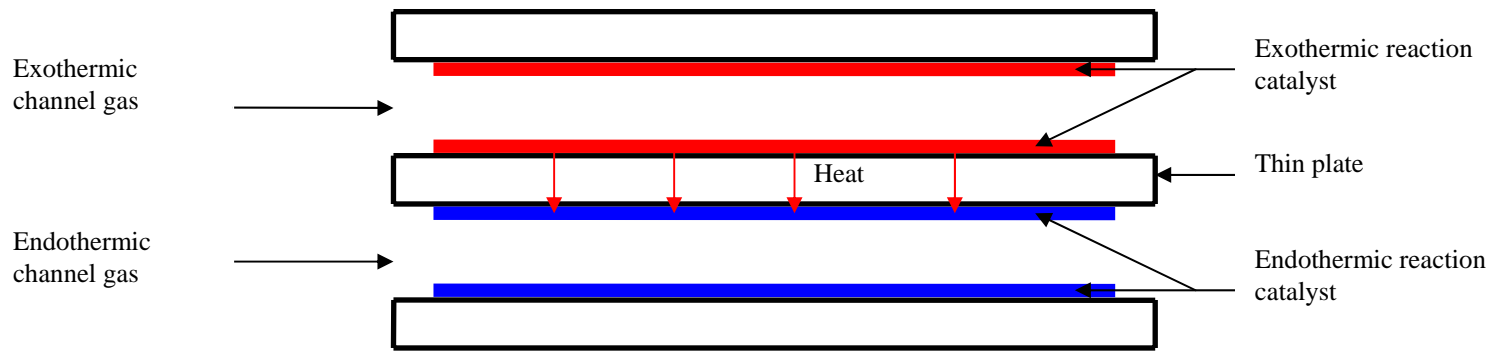
Typical Steam Cracking Furnaces

- Total Number of cracking tubes about 600
- Total Reaction Volume about 45 m³
- Total firebox volume about 9,000 m³
- Residence Time 0.25 to 0.75 s
- Firebox Efficiency about 65%



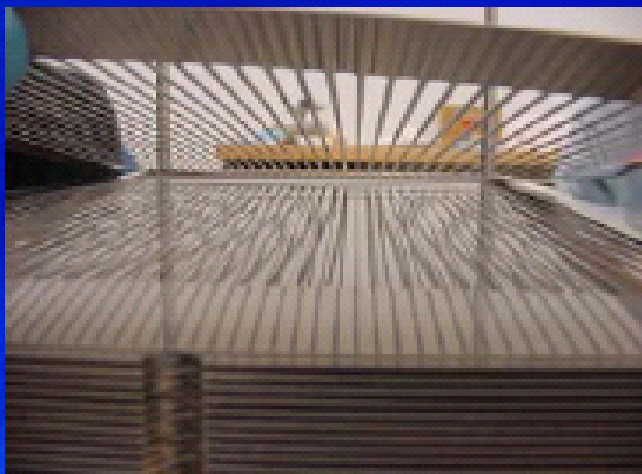
Steam function and process limitation

- ❑ Enhance heat transfer
- ❑ Reduce coke formation and deposition
- ❑ Improve selectivity towards ethylene
- ❑ Operation purposes
- ❑ Coke deposition is the main process limitations due to:
 - High tube skin temperature
 - High pressure drop



Catalytic Plate Reactor

Velocys Device Fabrication



Source: Velocys,(2005),olefins by high intensity oxidation, <http://www.velocys.com/lmg/pdf.2250.pdf>

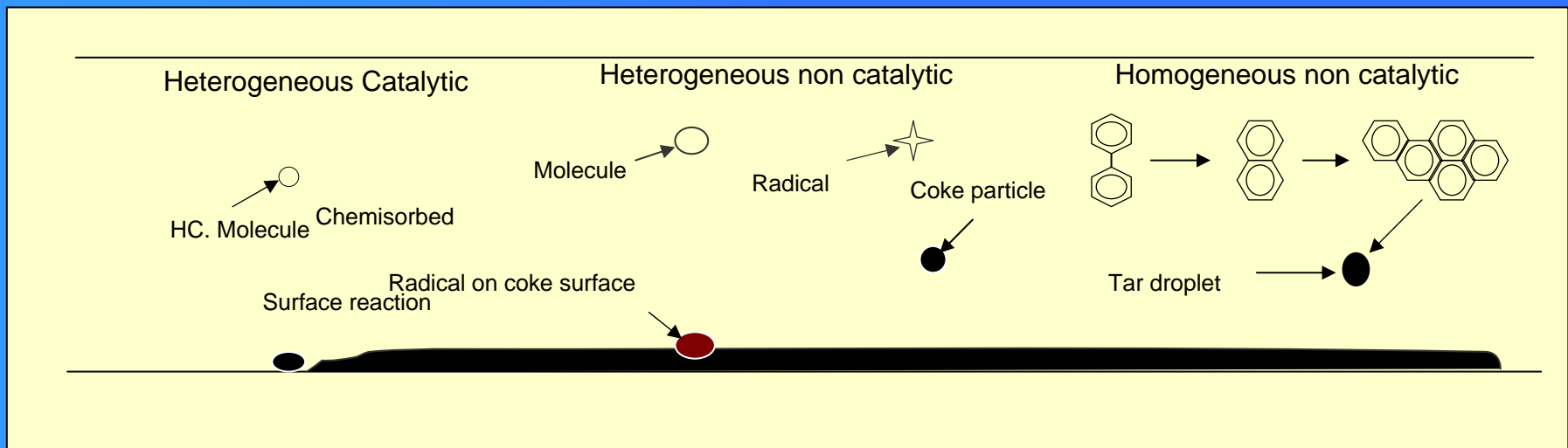


Advantages Of Catalytic Plate Reactor

- ❑ High Surface to volume Ratio
- ❑ Laminar flow Conditions
- ❑ High Heat transfer Coefficient
- ❑ Thin Catalyst Layer Minimize Diffusion Limitation
- ❑ Surface Temperature only few degrees above the process temperature
- ❑ Improved Safety and Environmental Impact
- ❑ Scale-up by Numbering –up
- ❑ Low Capital and operating Costs

Coke formation

- ❑ Metal-catalyzed coke
- ❑ Non-catalytic coke from tars
- ❑ Small chemical species (coke precursors) react with free radicals on the coke surface





Objectives

- 1- Study and investigate the possibility of intensifying the thermal cracking of propane to produce ethylene through the use of the catalytic plate reactors.
- 2- Reducing the coke formation and deposition.
- 3- Reducing the use of steam.
- 4- Modelling and simulation for propane cracking using Catalytic Plate Reactor.



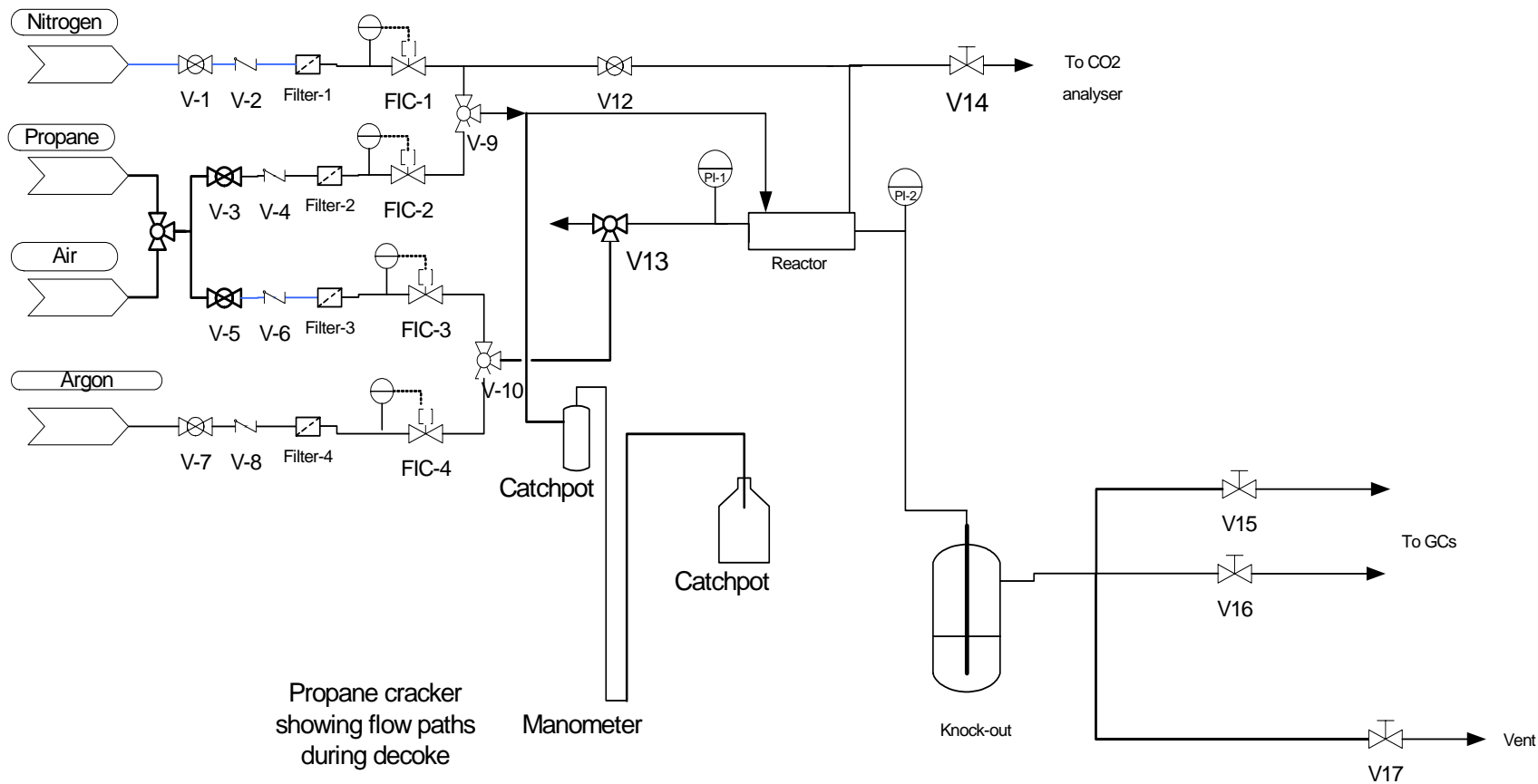
Benefits

- ❑ Lower environmental and safety impacts.
(NO_x, contaminated water, CO₂, H₂S)
- ❑ Improved energy efficiency.
- ❑ Lower capital cost.
- ❑ Improved overall plant economics



Experimental setup design criteria

- ❑ Allows for accurate coke measurement
- ❑ Constant and uniform temperature along the reactor
- ❑ Very fast cooling of reaction products
- ❑ Easy to change reactor size and material

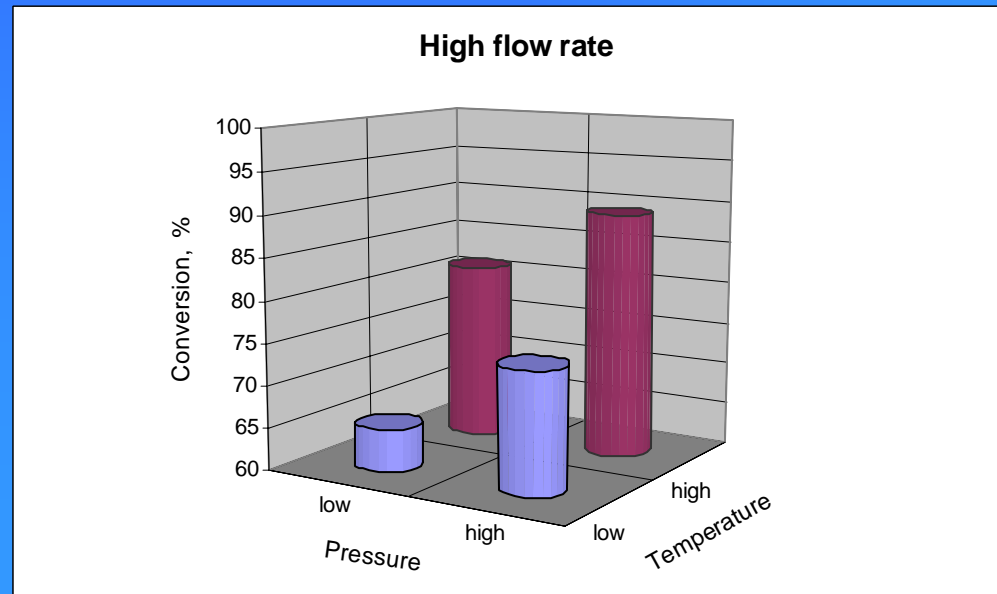
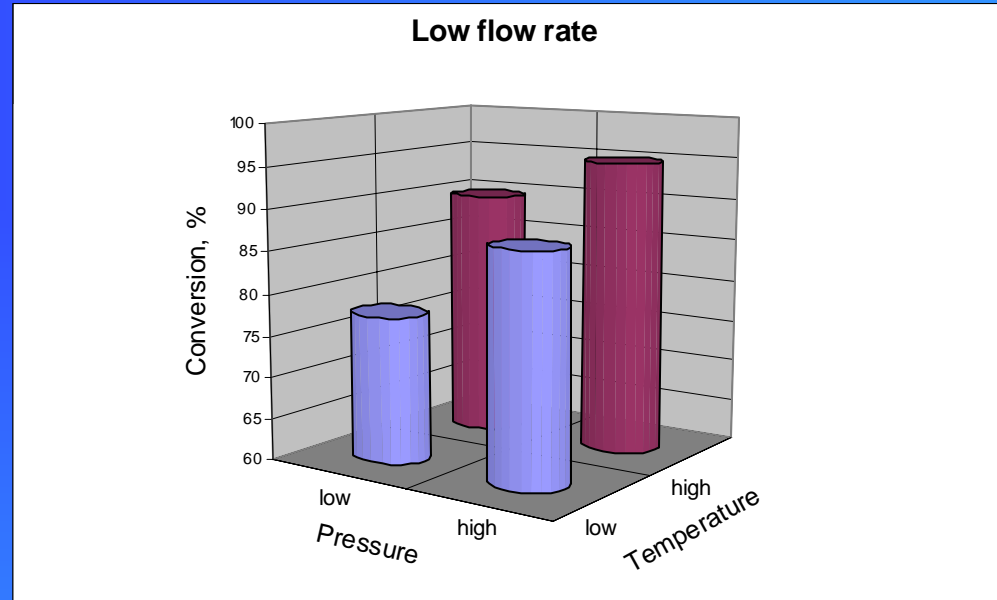




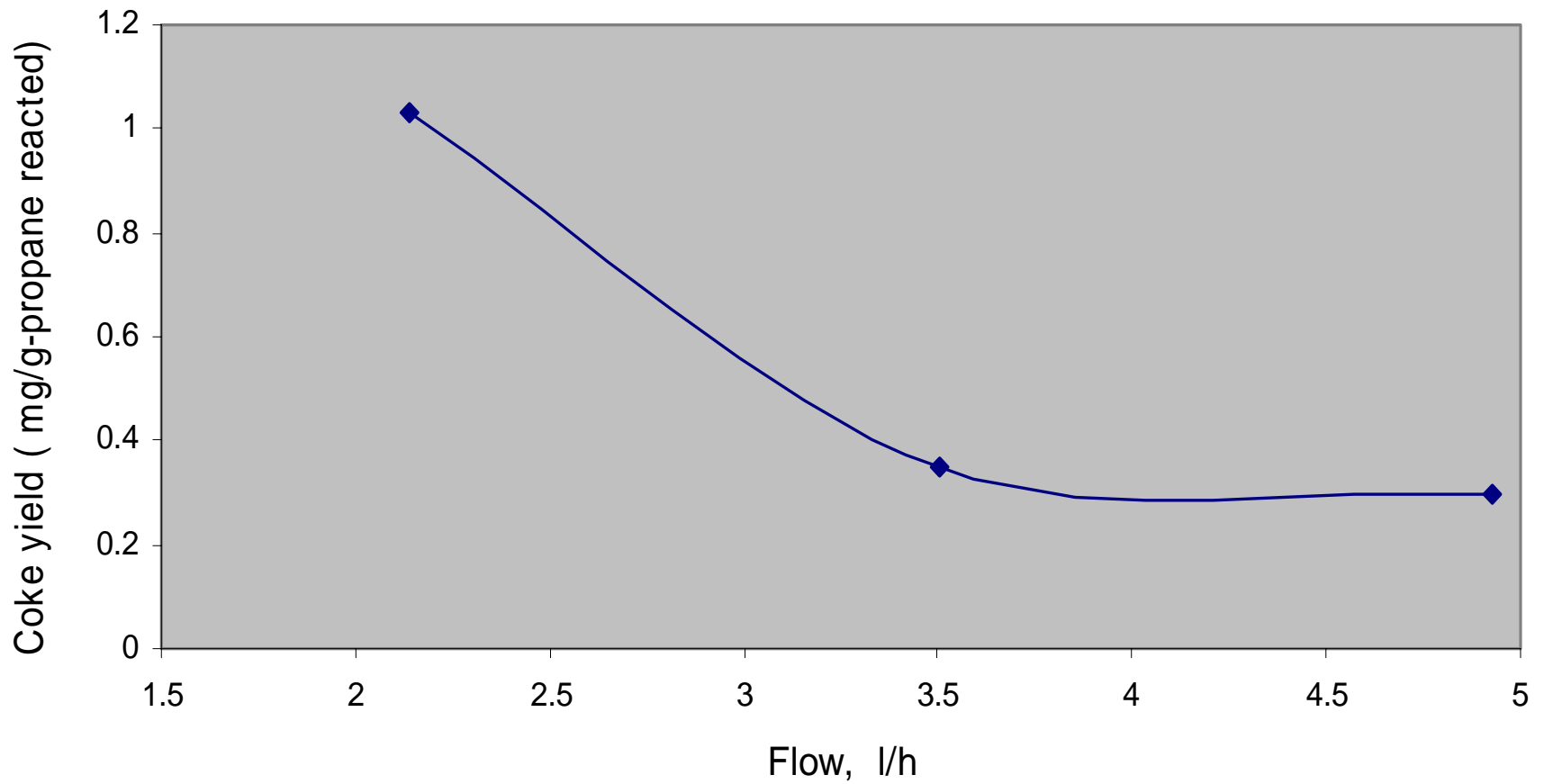
Experimental variables

- Reactor materials and internal coatings
- Reactor channel size
- Process variables (temperature, pressure, and flow rate)
- Run time length

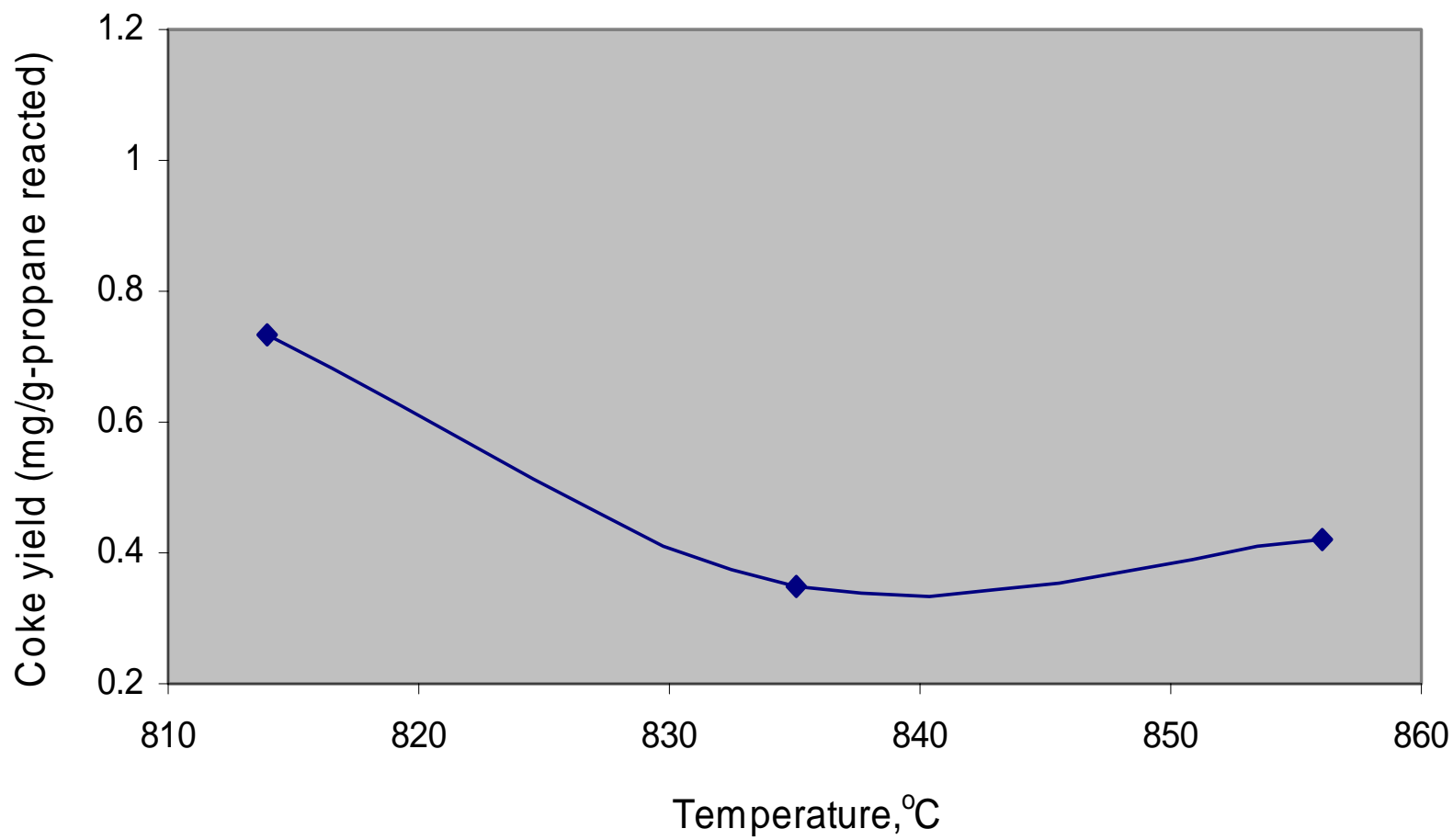
Conversion at low and high operating parameters



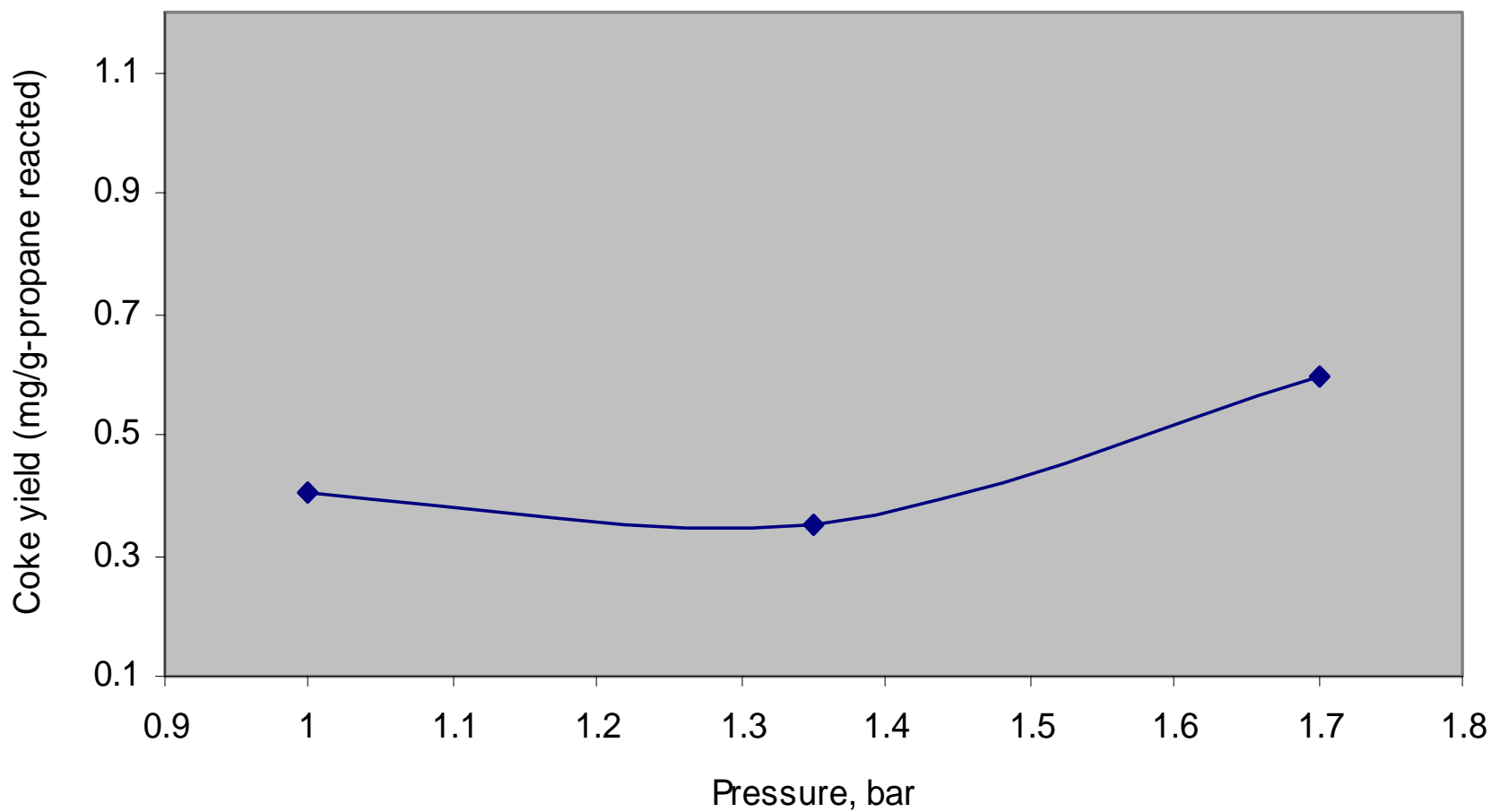
Coke yield vs Flow at 835 °C and 1.35 bar



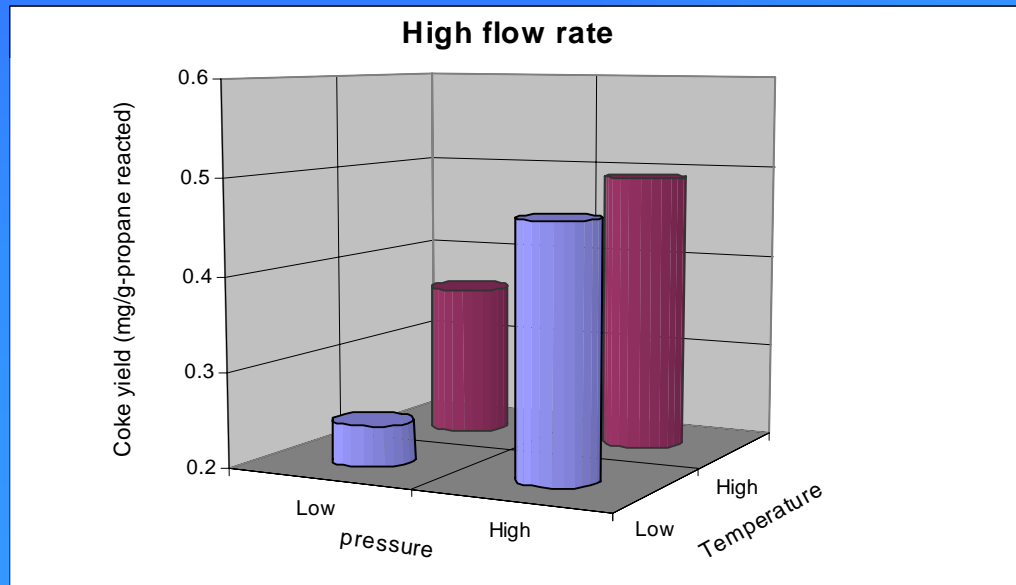
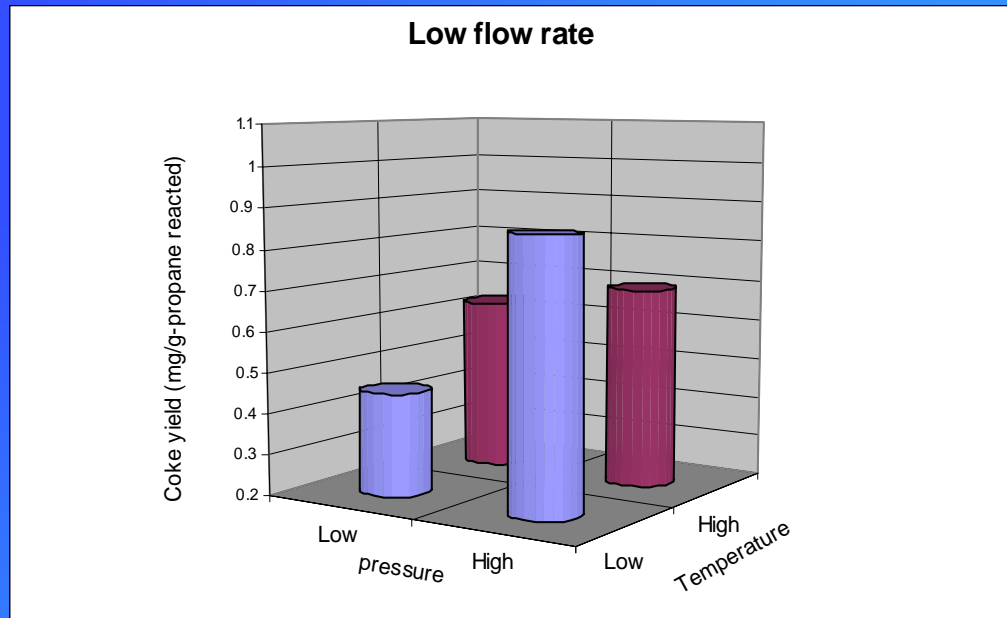
Coke yield vs Temperature. at 3.5 l/h and 1.35 bar



Coke yield vs Pressure at 3.5 l/h and 835 °C



Coke yield at low and high operating parameters



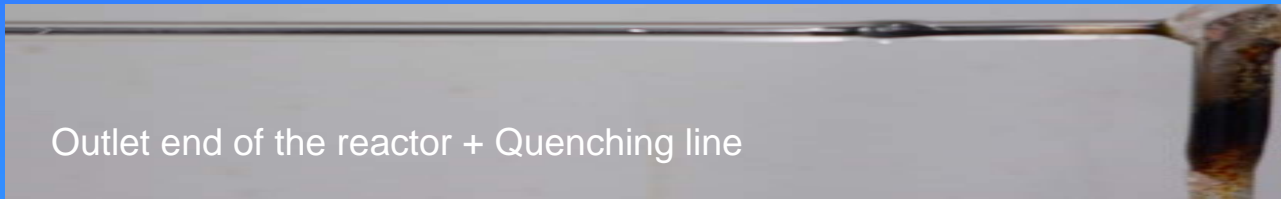
Inlet of the reactor



Middle of the reactor

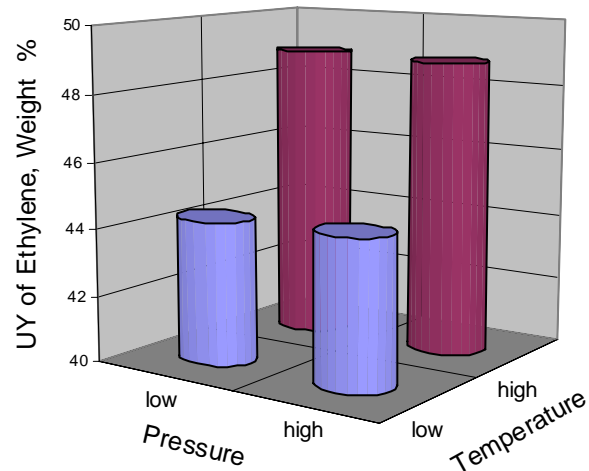


Outlet end of the reactor + Quenching line



UY of Ethylene at low and high operating parameters

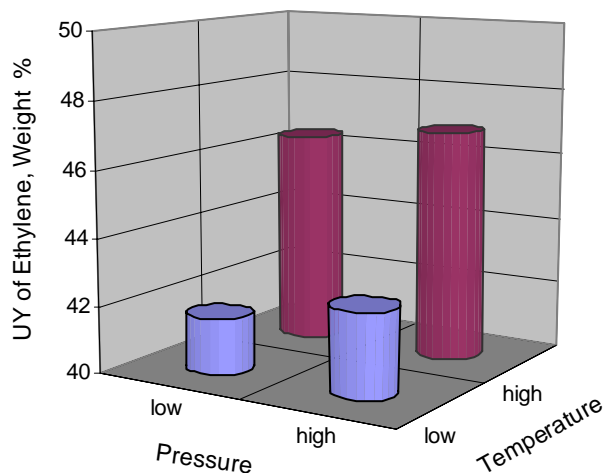
Low flow rate



$$\text{Ultimate Yield} = \frac{\text{Mass Ethylene Produced}}{\text{Mass Propane In Feed}}$$

Assuming that the unreacted propane and the ethane produced by one pass through the reactor, are recycled to the feed

High flow rate



Conclusions

- Conversion of about 90 % can be achieved in 2 mm internal diameter fused silica reactor without any significant pressure drop.
- Steam use can be reduced or possibly eliminated.
- High olefins yield can be obtained without steam.
- Low acetylene and C_4^+ yield.
- Run length of about 14 – 20 days was estimated to be possible before any decoking is required. This run length was achieved with no steam.

THANK YOU